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# Catalytic Compositions Based on Chlorides of *d* Metals and Natural Aluminosilicates for the Low-Temperature Sulfur Dioxide Oxidation with Air Oxygen

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Samples of natural bentonite and clinoptilolite modified with copper(II), iron(III), and palladium(II) were characterized by both X-ray phase and the Fourier transform infrared spectral methods. The activity of monometallic compositions  $M_iL_j/S$  ( $M = \text{Co(II)}, \text{Fe(III)}, \text{and Pd(II)}$ ;  $L = \text{NO}_3^-, \text{Cl}^-, \text{and SO}_4^{2-}$ ;  $S = \text{N-CLI or N-Bent}$ ) in the reaction with sulfur dioxide was found to depend on the nature of both a metal ion and a support. For bimetallic compositions  $\text{Cu(II)-Fe(III)}$  and  $\text{Cu(II)-Pd(II)}$  based on the natural aluminosilicates, a certain synergism in the action of metals forming these pairs towards the reaction of sulfur dioxide oxidation with oxygen was determined.

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## 1. Introduction

In spite of the fact that there are some works [1, 2] concerning sulfur dioxide, the most widespread atmospheric pollutant, abatement in air, this problem remains relevant as before because the recent metal and oxide catalysts (except for those containing manganese oxides [3]) are active only at high temperatures and are not suitable for application at ambient temperature. Some salts of *d* metals such as iron, copper, manganese, and cobalt dissolved in water [4] are able to oxidize sulfur dioxide at its concentrations of  $10^{-7} \div 10^{-6}$  mol/l at room temperature. We would like to notice that the simultaneous presence of two metal ions may cause their simple additive action (for  $\text{Mn(II)-Ni(II)}$  [5]), their synergetic action (for  $\text{Mn(II)-Fe(III)}$ ,  $\text{Mn(II)-Co(II)}$  [6], and  $\text{Cu(II)-Fe(III)}$  [7]), or the inhibition of their action (for  $\text{Mn(II)-Cr(III)}$  [5]). The detailed kinetic and thermodynamic analysis of numerous data on the liquid phase sulfur(IV) oxidation in the equilibrium mixture  $\text{SO}_{2aq} - \text{HSO}_3^- - \text{SO}_3^{2-}$  as well as the possible theoretic interpretation of synergetic action of *d* metal ions in this process are reported in works of Ermakov et al. [8–10], Golodov [11], and some former but still relevant papers [5–7].

It is well-known that the reactivity of metal ions can be altered by their anchoring on different supports but there are only few works [2, 12, 13] investigating compositions thus obtained in their reactions with sulfur dioxide. Such compositions consist of  $\text{Co}^{2+}$ ,  $\text{Mn}^{2+}$ ,  $\text{Cu}^{2+}$ ,  $\text{Fe}^{2+}$ ,  $\text{Fe}^{3+}$  or  $\text{Ag}^+$  and such supports as zeolites (clinoptilolite [2] and NaY [13]). These compositions have no catalytic activity and, after certain periods of time,  $\text{SO}_2$  concentration at

the reactor outlet attains its initial value. The only information on the catalysts consisting of metal complexes anchored on natural minerals for sulphur dioxide oxidation with air oxygen is presented in our earlier work [14].

The aim of this work was to find conditions under those mono- and bimetallic compositions anchored on natural aluminosilicates, i.e. bentonite and clinoptilolite, show their catalytic performance in the reaction of low-temperature sulphur dioxide oxidation with air oxygen.

## 2. Experimental

Such compositions as  $M_iL_j/S$  ( $S = \text{N-Bent}$  and  $\text{N-CLI}$ ;  $M = \text{Cu}^{2+}, \text{Fe}^{3+}, \text{Pd}^{2+}$ ;  $L = \text{Cl}^-, \text{NO}_3^-, \text{and SO}_4^{2-}$ ), and  $\text{CuCl}_2 - M_iL_j/S$  ( $M = \text{Fe}^{3+}$  or  $\text{Pd}^{2+}$ ) were prepared by a method of incipient wetness impregnation of natural bentonite (Dashukovskoye deposit, Ukraine) and natural clinoptilolite (Sokirnitskoye deposit, Ukraine) with aqueous-alcoholic solutions of corresponding salts. The samples thus obtained were dried in air at  $20^\circ\text{C}$  till constant weight.

The X-ray diffraction phase analysis was carried out on a Siemens D500 diffractometer ( $\text{CuK}\alpha$  radiation,  $\lambda = 1.54178 \text{ \AA}$ ) with a secondary beam graphite monochromator [14, 15].

Infrared analysis was carried out using a Fourier transform infrared spectrometer (PerkinElmer FT-IR spectrometer) with resolution of  $4 \text{ cm}^{-1}$  [14, 15].

A gas-air mixture (GAM) with  $\text{SO}_2$  concentration of  $150 \text{ mg/m}^3$  was obtained by mixing a purified air flow and a flow of pure  $\text{SO}_2$  in a special mixer. Initial and final sulphur dioxide concentrations,  $C_{\text{SO}_2}^{\text{in}}$  and  $C_{\text{SO}_2}^{\text{f}}$ , respectively, were measured using a 667EKh08 electrochemical gas analyzer (made by "Analitpribor", Ukraine) with the minimal detectable  $\text{SO}_2$  concentration of  $2 \text{ mg/m}^3$ .

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The kinetics of sulphur dioxide removal by the compositions under study was investigated using a gas flow setup with a fixed-bed glass reactor temperature-controlled at 293 K. The relative humidity of the GAM,  $\varphi_{GAM}$ , was kept at 76%. The weight of each sample under study was 10 g. The volume flow rate  $w$  of the GAM (1 l/min), the linear velocity  $U$  of the GAM (4.2 cm/s), and the ratio between the average grain size of aluminosilicate samples  $\bar{d}_g$  (0.75 mm) and an inner diameter of the reactor met the requirements for the regime of ideal displacement and the reaction proceeding in the kinetic region.

### 3. Results and discussion

#### 3.1. Results of physicochemical study of the supports and compositions based on them

X-ray phase analysis shows that the main phase of natural bentonite is montmorillonite characterized by the following values of X-ray spectral parameters  $2\theta$  and  $(d [\text{\AA}])$ :  $5.739^\circ$  (15.540),  $19.743^\circ$  (4.493),  $35.830^\circ$  (2.504),  $61.710^\circ$  (1.501). Besides the main phase, natural bentonite contains  $\alpha$ -quartz and calcite. The polyphase composition of N-Bent is confirmed by data of its Fourier transform infrared (FT-IR) spectrum containing absorption bands at 3692, 3622, 1036, 915, 876, 519, and  $468 \text{ cm}^{-1}$  characteristic of montmorillonite structural groups and also the shoulders of amorphous  $\text{SiO}_2$  at 1163 and  $1096 \text{ cm}^{-1}$ , the bands of  $\alpha$ -quartz at 799, 779, and  $695 \text{ cm}^{-1}$  and the band of calcite at  $1421 \text{ cm}^{-1}$ . Very low concentrations of metal salts ( $10^{-7}$ - $10^{-5} \text{ mol/g}$ ) in the compositions are not able to create some evident changes both in X-ray and FT-IR spectra.

The pure clinoptilolite phase in natural clinoptilolite is identified based on three base reflections at  $2\theta$  and  $(d [\text{\AA}])$ :  $9.856^\circ$  (8.959),  $22.416^\circ$  (3.963),  $30.057^\circ$  (2.970). Impurity phases are  $\alpha$ -quartz, mordenite, and  $\text{Fe}_2\text{O}_3$ . It should be noted that for compositions based on clinoptilolite as well as for those based on bentonite there are no changes induced by anchored metal salts. However, the IR spectra of N-CLI change as a result of Cu(II) and Pd(II) salts anchoring. These alterations are observed in the region of vibrations characteristic of OH groups bound to adsorbed water molecules (the shift from 3444 to  $3427 \text{ cm}^{-1}$ ) and vibrations characteristic of Brønsted OH groups in Si(OH)Al bridges (the shift from 3625 to  $3618 \text{ cm}^{-1}$ ). Such alterations could be explained by formation of surface metal complexes.

#### 3.2. Results of kinetic study

Compositions based on both aluminosilicates were tested in the reaction of  $\text{SO}_2$  oxidation with air oxygen. In the case of bentonite based monometallic compositions  $\text{M}_i\text{L}_j/\text{N-Bent}$ , where  $\text{M} = \text{Fe(III)}, \text{Cu(II)}, \text{Pd(II)}$  and  $\text{L} = \text{NO}_3^-, \text{Cl}^-, \text{SO}_4^{2-}$  it was found that their activity in the reaction with sulphur dioxide depended on the nature of both metal and anion. As an example, the influence of anion was demonstrated for Fe(III) salts. Figure 1 shows curves  $C_{\text{SO}_2}^f$  vs. time ( $\tau$ ) obtained as a result

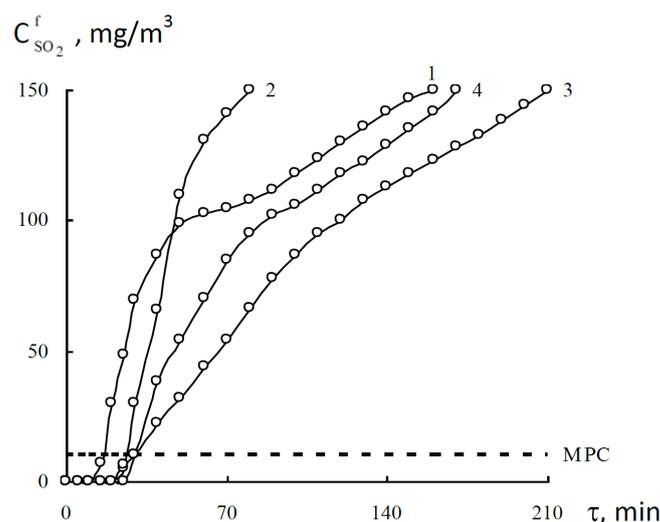


Fig. 1. Time dependence of  $C_{\text{SO}_2}^f$  in the course of sulfur dioxide removal from air with N-Bent (1),  $\text{Fe}(\text{NO}_3)_3/\text{N-Bent}$  (2),  $\text{FeCl}_3/\text{N-Bent}$  (3), and  $\text{Fe}_2(\text{SO}_4)_3/\text{N-Bent}$  (4) ( $C_{\text{Fe(III)}} = 1.0 \times 10^{-6} \text{ mol/g}$ ).

of GAM passing through fixed beds of N-Bent and Fe(III) containing monometallic compositions based on it.

Analyzing the experimental data, we use kinetic and stoichiometric reaction parameters:  $\tau_0$ ,  $\tau_{MPC}$ ,  $\tau_{1/2}$ , and  $Q_{exp}$ .  $\tau_0$  is a period of time when  $\text{SO}_2$  is completely removed from GAM, i.e. when  $C_{\text{SO}_2}^f = 0$ ;  $\tau_{MPC}$  is a time of protective action, i.e. a period of time from experiment beginning up to the moment when  $C_{\text{SO}_2}^f$  achieves the maximum permissible concentration of sulphur dioxide equal to  $10 \text{ mg/m}^3$ ;  $\tau_{1/2}$  is a half-conversion time, i.e. a period of time from experiment beginning up to the moment when  $C_{\text{SO}_2}^f$  became equal to  $0.5C_{\text{SO}_2}^{in}$ ;  $Q_{exp}$  is an amount of  $\text{SO}_2$  (mol) entering into the reaction during a total period of testing.

It is obvious that all kinetic curves presented have portions characterized by the complete removal of  $\text{SO}_2$  and then  $C_{\text{SO}_2}^f$  goes up and becomes equal to  $C_{\text{SO}_2}^{in}$ . All kinetic and stoichiometric reaction parameters mentioned above increase in the order N-Bent(1) <  $\text{Fe}(\text{NO}_3)_3/\text{N-Bent}$  <  $\text{FeCl}_3/\text{N-Bent}$  <  $\text{Fe}_2(\text{SO}_4)_3/\text{N-Bent}$ . Kinetic curves for bentonite anchored Cu(II) and Pd(II) salts are similar to those presented in Fig. 1. The most active compositions of these metals are  $\text{CuCl}_2/\text{N-Bent}$  and  $\text{PdCl}_2/\text{N-Bent}$ . By varying a concentration of copper(II) chloride in  $\text{CuCl}_2/\text{N-Bent}$  from  $1.5 \times 10^{-5}$  to  $2.9 \times 10^{-4} \text{ mol/g}$ , we have found that  $\tau_{MPC}$  increases from 25 to 55 min and  $Q_{exp}$  rises from  $1.13 \times 10^{-5}$  to  $2.81 \times 10^{-5} \text{ mol}$  of  $\text{SO}_2$ . For  $\text{PdCl}_2/\text{N-Bent}$ ,  $\tau_0$ ,  $\tau_{MPC}$ ,  $\tau_{1/2}$ , and  $Q_{exp}$  parameters are practically unchanged when palladium(II) concentration increases from  $1.5 \times 10^{-6}$  to  $6.8 \times 10^{-6} \text{ mol/g}$ , however, these parameters are higher than for N-Bent. Interestingly, the parameters became lower than for N-Bent when  $C_{\text{Pd(II)}} > 6.8 \times 10^{-6} \text{ mol/g}$ .

As for mono- and bimetallic N-Bent based compositions (Fig. 2 and Table I), all of them demonstrate rather high adsorption properties towards sulfur dioxide

and some of them (5, 7, and 8) show certain periods of time when  $C_{\text{SO}_2}^f$  is constant that is characteristic of a steady state mode.

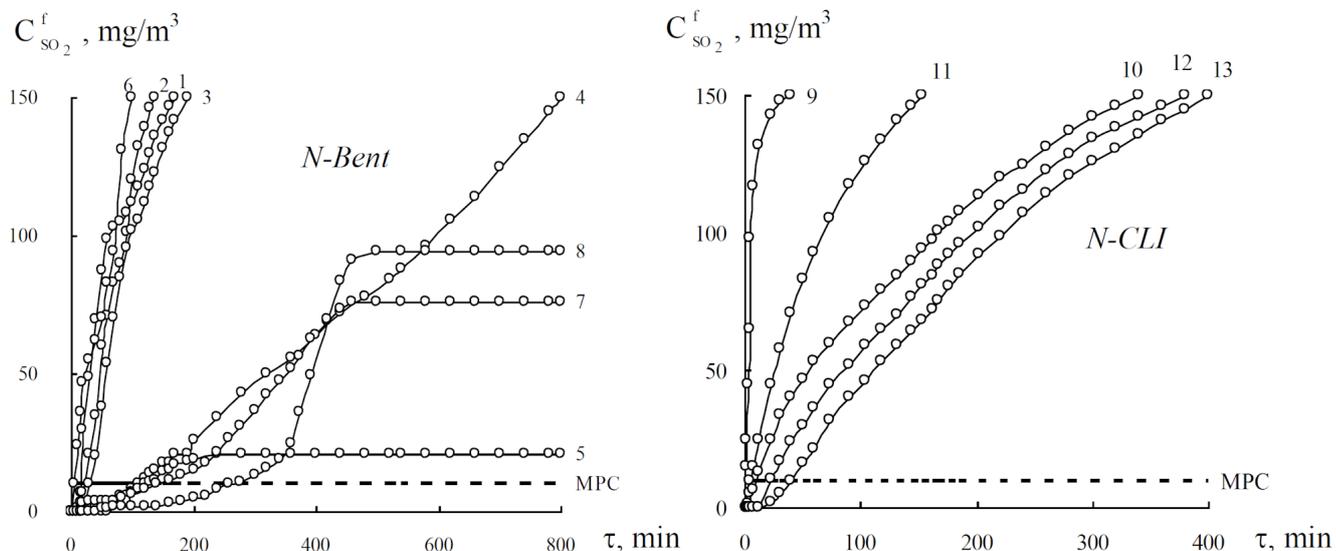


Fig. 2. Time dependence of  $C_{\text{SO}_2}^f$  characteristic of sulfur dioxide removal with N-Bent (1) and N-CLI (9) as well as its oxidation with air oxygen over  $\text{CuCl}_2/\text{N-Bent}$  (2),  $\text{FeCl}_3/\text{N-Bent}$  (3),  $\text{CuCl}_2\text{-FeCl}_3/\text{N-Bent}$  (4),  $\text{CuCl}_2\text{-FeCl}_3\text{-KCl}/\text{N-Bent}$  (5),  $\text{K}_2\text{PdCl}_4/\text{N-Bent}$  (6),  $\text{CuCl}_2\text{-K}_2\text{PdCl}_4/\text{N-Bent}$  (7),  $\text{CuCl}_2\text{-K}_2\text{PdCl}_4\text{-KCl}/\text{N-Bent}$  (8);  $\text{CuCl}_2/\text{N-CLI}$  (10),  $\text{K}_2\text{PdCl}_4/\text{N-CLI}$  (11),  $\text{CuCl}_2\text{-K}_2\text{PdCl}_4/\text{N-CLI}$  (12),  $\text{CuCl}_2\text{-K}_2\text{PdCl}_4\text{-KCl}/\text{N-CLI}$  (13).

TABLE I

Parameters of sulfur dioxide removal from air with natural aluminosilicates as well as its oxidation with air oxygen over compositions containing  $d$  metal chlorides and based on these natural supports  $C_{\text{Pd(II)}} = 2.72 \times 10^{-5}$ ,  $C_{\text{Cu(II)}} = 5.9 \times 10^{-5}$ ,  $C_{\text{Fe(III)}} = 1.0 \times 10^{-6}$  mol/g,  $t = 20^\circ\text{C}$ ,  $C_{\text{SO}_2}^{\text{in}} = 150$  mg/m<sup>3</sup>.

Composition number*	Composition	$\tau_0$ [min]	$\tau_{\text{MPC}}$ [min]	$\tau_{1/2}$ [min]	$Q_{\text{exp}} \times 10^4$ [mol SO <sub>2</sub> ]	$K_s$
1	N-Bent	10	15	35	1.11	-
2	$\text{CuCl}_2/\text{N-Bent}$	15	25	55	1.20	-
3	$\text{FeCl}_3/\text{N-Bent}$	25	30	65	1.57	-
4	$\text{CuCl}_2\text{-FeCl}_3/\text{N-Bent}$	30	110	460	10.20	2.0
5	$\text{CuCl}_2\text{-FeCl}_3\text{-KCl}/\text{N-Bent}$	60	120	-	16.30**	2.2
6	$\text{K}_2\text{PdCl}_4/\text{N-Bent}$	1	5	30	0.77	-
7	$\text{CuCl}_2\text{-K}_2\text{PdCl}_4/\text{N-Bent}$	5	140	440	12.30**	4.7
8	$\text{CuCl}_2\text{-K}_2\text{PdCl}_4\text{-KCl}/\text{N-Bent}$	40	260	420	12.10**	8.7
9	N-CLI	-	-	5	0.09	-
10	$\text{CuCl}_2/\text{N-CLI}$	4	10	110	2.60	-
11	$\text{K}_2\text{PdCl}_4/\text{N-CLI}$	2	5	45	1.02	-
12	$\text{CuCl}_2\text{-K}_2\text{PdCl}_4/\text{N-CLI}$	12	25	145	3.20	1,7
13	$\text{CuCl}_2\text{-K}_2\text{PdCl}_4\text{-KCl}/\text{N-CLI}$	12	40	170	3.80	2,7

\* composition numbers coincide with numbers of curves in Fig.2

\*\* the experiment was stopped in 800 min

Making a comparison between the two aluminosilicates under study (Fig. 2 and Table I), one can see that the kinetics of SO<sub>2</sub> adsorption from GAM by natural clinoptilolite (curve 9) is quite different compared with that for natural bentonite (curve 1), i.e., for N-CLI, in contrast

to N-Bent, there is no period of time when SO<sub>2</sub> removal is complete,  $\tau_0$ , and the total amount of SO<sub>2</sub> adsorbed by N-CLI ( $0.9 \times 10^{-5}$  mol) is much less than that in the case of N-Bent.

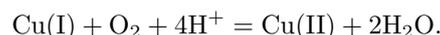
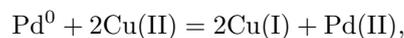
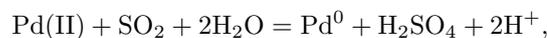
For palladium(II) and copper(II) monometallic compositions based on N-Bent and N-CLI, kinetic curves are similar: at the beginning,  $\tau_0$  portions of curves are present and a consequent gradual increase in  $C_{\text{SO}_2}^f$  up to  $C_{\text{SO}_2}^{\text{in}}$  takes place. A similar shape of kinetic curves for  $\text{SO}_2$  adsorption by  $\text{M}^{n+}/\text{N-CLI}$  compositions ( $\text{M}^{n+} = \text{Zn}^{2+}, \text{Co}^{2+}, \text{Cd}^{2+}, \text{Mn}^{2+}, \text{Cu}^{2+}, \text{Fe}^{2+}, \text{Ag}^+, \text{Ca}^{2+}, \text{Li}^+, \text{Na}^+, \text{K}^+$ ) obtained by the ion-exchange method was described earlier [2]. It is evident (Table I) that  $\tau_0$  and  $\tau_{\text{MPC}}$  parameters for  $\text{CuCl}_2/\text{N-CLI}$  are lower than those for  $\text{CuCl}_2/\text{N-Bent}$ , whereas these parameters do not change and are the same for  $\text{Pd(II)}/\text{N-CLI}$  and  $\text{Pd(II)}/\text{N-Bent}$ . Interestingly,  $\tau_{1/2}$  and  $Q_{\text{exp}}$  parameters for  $\text{M}^{2+}/\text{N-CLI}$  are higher than those for  $\text{M}^{2+}/\text{N-Bent}$  ( $\text{M}^{2+} = \text{Cu}^{2+}, \text{Pd}^{2+}$ ).

In the case of bimetallic compositions based on the two aluminosilicates, the kinetic curves characterized by the presence of  $\tau_0$  portions and consequent gradual increases in  $C_{\text{SO}_2}^f$  up to  $C_{\text{SO}_2}^{\text{in}}$  are also observed for bimetallic compositions 12 ( $\text{Cu(II)-Pd(II)}/\text{N-CLI}$ ) and 13 (in fact, composition 12 doped with chloride ions) as well as for bimetallic composition 4 ( $\text{CuCl}_2\text{-FeCl}_3/\text{N-Bent}$ ) (Fig. 2). Compositions 4, 12, and 13 are much more active (i.e. their reaction parameters are noticeably higher) than their monometallic counterparts but they do not demonstrate a steady-state mode of sulfur dioxide oxidation. N-Bent based bimetallic compositions 5, 7, and 8 show that the reaction kinetics substantially differed from that for bimetallic composition 4, 12, and 13. As can be seen from Fig. 2, kinetic curves demonstrating the behavior of compositions 5, 7, and 8 show long portions with  $C_{\text{SO}_2}^f = \text{const}$  characteristic of a steady-state mode and indicating the true catalytic process of sulfur dioxide oxidation. Notably, composition 5 containing additional chloride ions ( $C_{\text{KCl}} = 6.8 \times 10^{-6}$  mol/g) shows the true catalytic action in contrast to composition 4 not containing additional chloride ions. At the same time, additional chloride ions worsen the catalytic action for composition 8 ( $\text{SO}_2$  oxidation level decreases) as compared with composition 7. For the  $\text{Cu(II)-Pd(II)}/\text{N-CLI}$  compositions, additional chloride ions in composition 13 ( $\text{Cu(II)-Pd(II)}/\text{N-CLI}$ ) make it slightly more active than composition 12 (Table I) although both compositions do not show a true catalytic behavior.

It is evident that all bimetallic compositions based on both N-Bent and N-CLI show the explicit synergetic action of two metal ions. This is confirmed by values of their synergetic factors,  $K_s$ , (calculated as a ratio of  $\tau_{\text{MPC}}$  for each bimetallic system to the sum of  $\tau_{\text{MPC}}$  for corresponding monometallic systems) which are higher than 1 (Table I).

In our opinion, the observable synergetic effect can be explained as follows. When a supported composition is comprised of a single metal ion and a support, the interaction of this ion with sulfur dioxide results in the reduction of the metal ion. Its reoxidation by air oxygen is a very slow process if it takes place at all. In contrast

to that, for some metal ion pairs, e.g.  $\text{Fe(III)-Cu(II)}$  and  $\text{Pd(II)-Cu(II)}$ , such a process occurs: a reduced metal ion (a catalyst) can be rapidly oxidized with the second metal ion (a cocatalyst). The cocatalyst, in its turn, due to its lower redox potential can be rapidly reoxidized with air oxygen. Thus, a scheme of the catalytic process under study can be considered as that comprised of three stages, e.g. for  $\text{Pd(II)-Cu(II)}$  [16]:



This scheme is similar to the scheme of well-known Wacker process used for oxidation of ethylene and carbon monoxide.

Differences in the action of  $\text{Pd(II)-Cu(II)}$  compositions based on bentonite and clinoptilolite confirm our viewpoint [16, 17] that the nature of the support substantially influences the process of surface complexing and therefore the catalytic activity of metal complexes formed by metal ions on different supports.

#### 4. Conclusions

Bimetallic compositions  $\text{CuCl}_2\text{-M}_i\text{Cl}_j/\text{S}$  ( $\text{M}$  is  $\text{Fe(III)}$  or  $\text{Pd(II)}$  and  $\text{S}$  is N-Bent or N-CLI) obtained by us showed certain dependences of their activity in the reaction with sulfur dioxide on the nature of the metal ion and support. All bimetallic compositions under study show certain synergism in action of two *d* metal ions towards  $\text{SO}_2$  oxidation (some of them show the true catalytic action). For  $\text{Cu(II)-Pd(II)}$  compositions based on the two natural aluminosilicates, at the same metal ions and their concentrations, their synergetic factors depend on the nature of the support.

#### References

- [1] Y. Mathieu, L. Tzanis, M. Soulard, J. Patarin, M. Vierling, M. Moliere, *Fuel Process. Technol.* **144**, 81 (2013).
- [2] E. Ivanova, B. Kuomanova, *J. Hazard. Mater.* **167**, 306 (2009).
- [3] J.W. Long, J.M. Wallace, G.W. Peterson, K. Huynh, *ACS Appl. Mater. Interf.* **8**, 1184 (2016).
- [4] W. Pasiuk-Bronikowska, T. Bronikowski, *Chem. Eng. Sci.* **44**, 1361 (1989).
- [5] R.K. Ulrich, G.T. Rochelle, R.E. Prada, *Chem. Eng. Sci.* **41**, 2183 (1986).
- [6] N. Coichev, K. Bal Reddy, R. van Eldik, *Atmos. Environ.* **26A**, 2295 (1992).
- [7] C.J. Weschler, M.L. Mandich, T.E. Graedel, *J. Geophys. Res.* **91**, 5189 (1986).
- [8] A.N. Ermakov, A.P. Purmal', *Kinet. Catalys.* **42**, 479 (2001).

- [9] A.N. Ermakov, A.P. Purmal', *Kinet. Catalys.* **43**, 249 (2002).
- [10] A.N. Yermakov, I.K. Larin, A.A. Ugarov, A.P. Purmal', *Kinet. Catalys.* **44**, 476 (2003).
- [11] V.A. Golodov, *Euras. ChemTech J.* **2**, 29 (2000).
- [12] H. Dathe, E. Peringer, V. Roberts, A. Jentys, J.A. Lercher, *C.R. Chimie* **8**, 753 (2005).
- [13] K.C. Khulbe, R.S. Mann, A. Manoogian, *Zeolites* **7**, 228 (1987).
- [14] T.L. Rakitskaya, E.V. Kameneva, T.A. Kiose, V.Y. Volkova, *Solid State Phenom.* **230**, 291 (2015).
- [15] T.L. Rakitskaya, T.A. Kiose, A.M. Zryutina, R.E. Gladyshevskii, A.S. Truba, V.O. Vasylechko, P.Y. Demchenko, G.V. Gryschouk, V.Y. Volkova, *Solid State Phenom.* **200**, 299 (2013).
- [16] T.L. Rakitskaya, A.A. Ennan, V.Y. Volkova, *Low-Temperature Catalytic Air Purification from Carbon Monoxide*, Ekologiya, Odessa 2005 (in Russian).
- [17] T.L. Rakitskaya, A.A. Ennan, *Phosphine Physicochemical Properties and Practical Aspects of Recovery*, Astroprint, Odessa 2012 (in Russian).